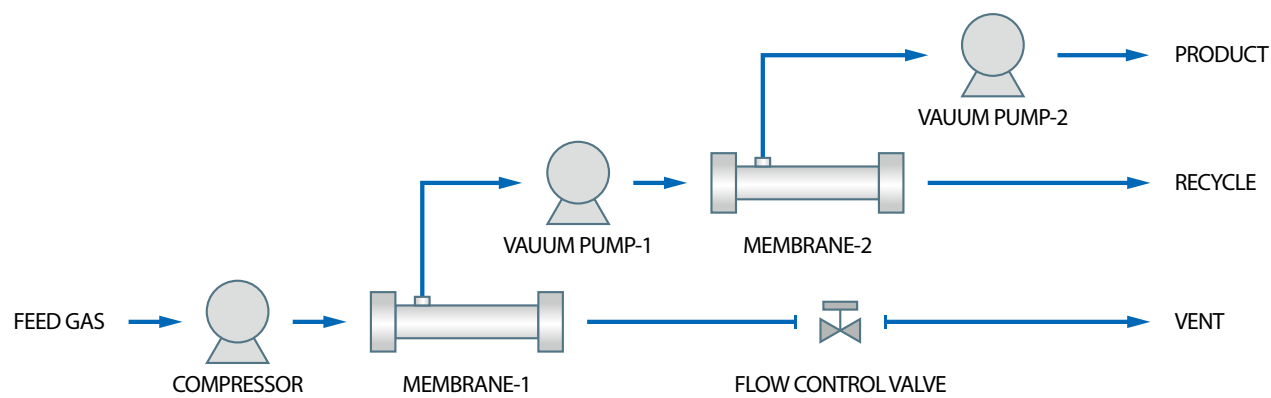


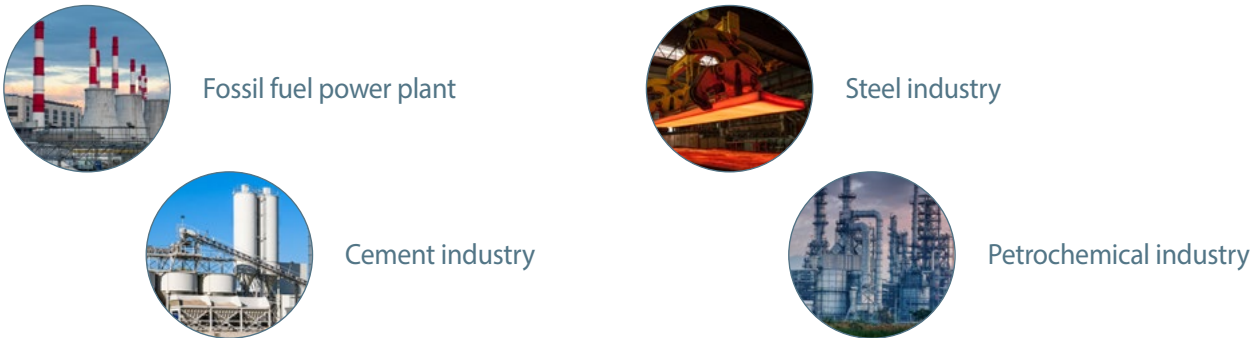
# CCUS & Clean H<sub>2</sub>

## Schematic Diagram



In order to prevent global climate change, technologies to reduce greenhouse gas emission is widely studied in the world. Airrane has been conducting research and development for many years to commercialize a membrane technology for CO<sub>2</sub> captures from flue gas emitted through stacks of various industries. As a result, Airrane commenced a project to supply a CO<sub>2</sub> separation membrane system to a commercial facility that collects 200,000 tons of CO<sub>2</sub> per year from a petrochemical plant flue gas. Based on this experience, we are expanding CO<sub>2</sub> capture business to power plants, steel mills, hydrogen production facilities and fuel cell power stations. The captured CO<sub>2</sub> through this process is liquefied and supplied to fresh food distributors, home shopping companies, and shipbuilders.

## Top CO<sub>2</sub> Disposal Industries



## Advantages of Membrane CCUS Technology

The CO<sub>2</sub> capture technologies are largely categorized in water-lean solvent method using liquid absorbent like amine or ammonia and membrane separation method. Each technology has advantages and disadvantages depending on the conditions of CO<sub>2</sub> emitting source. Membrane method is generally considered for higher CO<sub>2</sub> concentration source, while amine method is applied to lower CO<sub>2</sub> concentration. In reality, most of CCUS candidate locations need a retrofit designing because of the limited space to install. Membrane CCUS facility requires only 1/6 of the area compared to amine CCUS facility. On top of it, membrane is advantageous for resident acceptance and regulations like REACH.



Korea District Heating Corp.

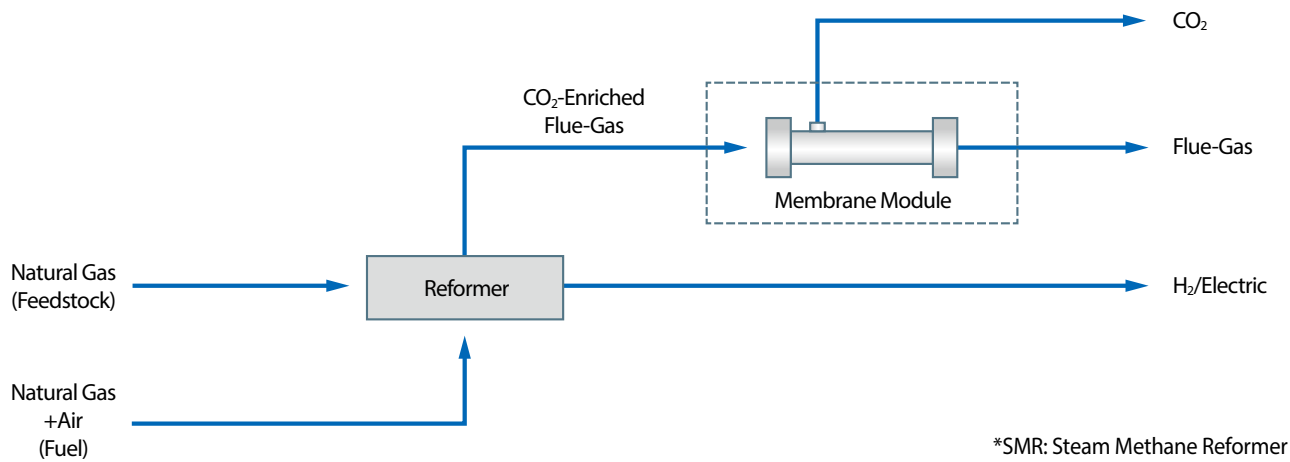


Lotte Chemical

## Membrane CCUS Demonstration Cases

| Item                    |                             | Coal Power Plant<br>Flue gas | LNG Power Plant<br>Flue gas | Cement Kiln<br>Flue gas | NCC Flue gas          |
|-------------------------|-----------------------------|------------------------------|-----------------------------|-------------------------|-----------------------|
| Site                    |                             | Daejeon                      | Pangyo, Suseo               | Okgye                   | Yeosu                 |
| Membrane Process Design |                             | 2stage                       | 3stage                      | 3stage                  | 3stage                |
| Feed                    | Feed gas amount             | 110m <sup>3</sup> /hr        | 400m <sup>3</sup> /hr       | 2,000m <sup>3</sup> /hr | 300m <sup>3</sup> /hr |
|                         | CO <sub>2</sub> Conc.       | 13.6~15%                     | 4.5~8%                      | 15~22.6%                | 13~14%                |
|                         | O <sub>2</sub> Conc.        | 0.7~3.4%                     | 5.5~12.8%                   | 9.9~14.3%               | 4~5%                  |
|                         | NOx                         | -                            | -                           | 45~54ppm                | ~ 50ppm               |
|                         | DUST                        | 15~22mg/m <sup>3</sup>       | ~2mg/m <sup>3</sup>         | serious                 | < 1mg/m <sup>3</sup>  |
| Product                 | CO <sub>2</sub> Conc.       | 83.9~84.2%                   | 65~84.9%                    | 85.4~90.4%              | 90~95%                |
|                         | CO <sub>2</sub> recovery(%) | 84~86.5%                     | 69~82%                      | 71~92%                  | 80%                   |

## Schematic Diagram of CO<sub>2</sub> Capture for SMR/H<sub>2</sub> Fuel Cell System



\*SMR: Steam Methane Reformer